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## 1.1 Derivation of Concentration Profile within a Porous Catalyst with a 1<sup>st</sup> Order Reaction

The concentration through a porous catalyst for a first order reaction can be described by the differential equation,

$$\frac{d^2 C_A}{dr^2} + \frac{2}{r} \frac{dC_A}{dr} - \frac{k_1'' S_a \rho_c}{D_e} C_A = 0 \quad (1.1.1)$$

This equation can be turned into a dimensionless version by defining 2 dimensionless variables,

$$\varphi = \frac{C_A}{C_{As}} \quad (1.1.2)$$

$$\lambda = \frac{r}{R} \quad (1.1.3)$$

This means that we can write,

$$r = \lambda R \quad (1.1.4)$$

$$dr = R d\lambda \quad (1.1.5)$$

and,

$$C_A = C_{As} \varphi \quad (1.1.6)$$

$$\frac{dC_A}{dr} = C_{As} \frac{d\varphi}{dr} \quad (1.1.7)$$

$$\frac{d^2 C_A}{dr^2} = C_{As} \frac{d^2 \varphi}{dr^2} \quad (1.1.8)$$

Combining with our definition of  $dr$  we then produce,

$$\frac{dC_A}{dr} = \frac{C_{As}}{R} \frac{d\varphi}{d\lambda} \quad (1.1.9)$$

$$\frac{d^2 C_A}{dr^2} = \frac{C_{As}}{R^2} \frac{d^2 \varphi}{d\lambda^2} \quad (1.1.10)$$

Substituting this into equation 1.1.1 produces,

$$\begin{aligned} \frac{C_{As}}{R^2} \frac{d^2 \varphi}{d\lambda^2} + \frac{2C_{As}}{\lambda R^2} \frac{d\varphi}{d\lambda} - \frac{k_1'' S_a \rho_c}{D_e} C_{As} \varphi &= 0 \\ \frac{d^2 \varphi}{d\lambda^2} + \frac{2}{\lambda} \frac{d\varphi}{d\lambda} - \frac{k_1'' S_a \rho_c R^2}{D_e} \varphi &= 0 \end{aligned} \quad (1.1.11)$$

We can now define a final dimensionless parameter,

$$\phi^2 = \frac{k_1'' S_a \rho_c R^2}{D_e} \quad (1.1.12)$$

Thus producing a dimensionless form of the differential equation for the concentration through a porous catalyst,

$$\frac{d^2 \varphi}{d\lambda^2} + \frac{2}{\lambda} \frac{d\varphi}{d\lambda} - \phi^2 \varphi = 0 \quad (1.1.13)$$

The boundary conditions can also be defined in terms of the dimensionless parameters<sup>1</sup>,

$$\begin{aligned} C_A = C_{As} \text{ at } r = R &\Rightarrow \varphi = 1 \text{ at } \lambda = 1 \\ \frac{dC_A}{dr} = 0 \text{ at } r = 0 &\Rightarrow \frac{d\varphi}{d\lambda} = 0 \text{ at } \lambda = 0 \end{aligned} \quad (1.1.14)$$

Equation 1.1.13 can be solved by defining a new variable  $y = \varphi\lambda$ , which means that,

$$\varphi = \frac{y}{\lambda} \quad (1.1.15)$$

$$\frac{d\varphi}{d\lambda} = \frac{1}{\lambda} \frac{dy}{d\lambda} - y \frac{1}{\lambda^2} \quad (1.1.16)$$

$$\begin{aligned} \frac{d^2\varphi}{d\lambda^2} &= \frac{1}{\lambda} \frac{d^2y}{d\lambda^2} - \frac{1}{\lambda^2} \frac{dy}{d\lambda} - \frac{1}{\lambda^2} \frac{dy}{d\lambda} + y \frac{2}{\lambda^3} \\ &= \frac{1}{\lambda} \frac{d^2y}{d\lambda^2} - \frac{2}{\lambda^2} \frac{dy}{d\lambda} + \frac{2}{\lambda^3} y \end{aligned} \quad (1.1.17)$$

Substituting these into equation 1.1.13 produces,

$$\begin{aligned} \frac{1}{\lambda} \frac{d^2y}{d\lambda^2} - \frac{2}{\lambda^2} \frac{dy}{d\lambda} + \frac{2}{\lambda^3} y + \frac{2}{\lambda^2} \frac{dy}{d\lambda} - \frac{2}{\lambda^3} y - \phi^2 \frac{1}{\lambda} y &= 0 \\ \frac{1}{\lambda} \frac{d^2y}{d\lambda^2} - \phi^2 \frac{1}{\lambda} y &= 0 \\ \frac{d^2y}{d\lambda^2} - \phi^2 y &= 0 \end{aligned} \quad (1.1.18)$$

This differential equation can now be solved by substituting an exponential form for  $y$  as,

$$y = e^{\beta\lambda} \quad (1.1.19)$$

where  $\beta$  is a value to find. Substituting this expression into equation 1.1.18 allows  $\beta$  to be calculated as,

$$\begin{aligned} \beta^2 e^{\beta\lambda} - \phi^2 e^{\beta\lambda} &= 0 \\ \beta^2 - \phi^2 &= 0 \\ (\beta - \phi)(\beta + \phi) &= 0 \\ \beta &= \pm \phi \end{aligned} \quad (1.1.20)$$

This means that from the linear combination of all solutions, then the full integrated expression can be given as,

$$y = Ae^{\phi\lambda} + Be^{-\phi\lambda} \quad (1.1.21)$$

or using the definition of  $y$ , equation 1.1.15,

$$\varphi = \frac{A}{\lambda} e^{\phi\lambda} + \frac{B}{\lambda} e^{-\phi\lambda} \quad (1.1.22)$$

<sup>1</sup>It should be noted here that if the reaction order is less than 1 it is possible to have what is called a dead zone, i.e. the concentration of the reactant drops to 0 before the centre of the catalyst, this means that the second boundary condition is not true in this case and needs to be replaced with  $\varphi = 0$  at  $\lambda = \lambda_c$  where  $\lambda_c$  has to be calculated from the balance equations. For example, see R. L. York, K. M. Bratlie, L. R. Hile, and L. K. Jang, (2011) *Catalysis Today*, 160:204-212.

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We can now use the boundary conditions, equation 1.1.14, to find the constants  $A$  and  $B$ . The differential of equation 1.1.22 is,

$$\frac{d\varphi}{d\lambda} = \frac{A}{\lambda^2} e^{\phi\lambda} (\phi\lambda - 1) - \frac{B}{\lambda^2} e^{-\phi\lambda} (\phi\lambda + 1) \quad (1.1.23)$$

Thus with our boundary condition at the centre of the particle we get,

$$\begin{aligned} 0 &= A(1)(-1) - B(1)(1) \\ A &= -B \end{aligned} \quad (1.1.24)$$

With this and our boundary condition at the surface of the particle we get,

$$\begin{aligned} 1 &= Ae^{\phi} + Be^{-\phi} \\ 1 &= A(e^{\phi} - e^{-\phi}) \\ 1 &= 2A \sinh \phi \\ A &= \frac{1}{2 \sinh \phi} = -B \end{aligned} \quad (1.1.25)$$

where we have used the mathematical definition of  $\sinh ax = \frac{e^{ax} - e^{-ax}}{2}$ . Substituting these constant values into equation 1.1.22 gives,

$$\begin{aligned} \varphi &= \frac{1}{\lambda \sinh \phi} \left( \frac{e^{\phi\lambda} - e^{-\phi\lambda}}{2} \right) \\ \varphi &= \frac{1 \sinh \phi\lambda}{\lambda \sinh \phi} \end{aligned} \quad (1.1.26)$$