

$$\delta u_i = \frac{\partial u_i}{\partial x_j} \delta x_j$$

$$\delta u_i = \underbrace{\omega_{ij}} \delta x_j + \underbrace{\epsilon_{ij}} \delta x_j$$

$$\underbrace{\frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)}_{\text{rotation}} \quad \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} - \frac{\partial u_j}{\partial x_i} \right)$$

$\epsilon_{(ij)}$  = rate of strain in  $x_i$ -direct.

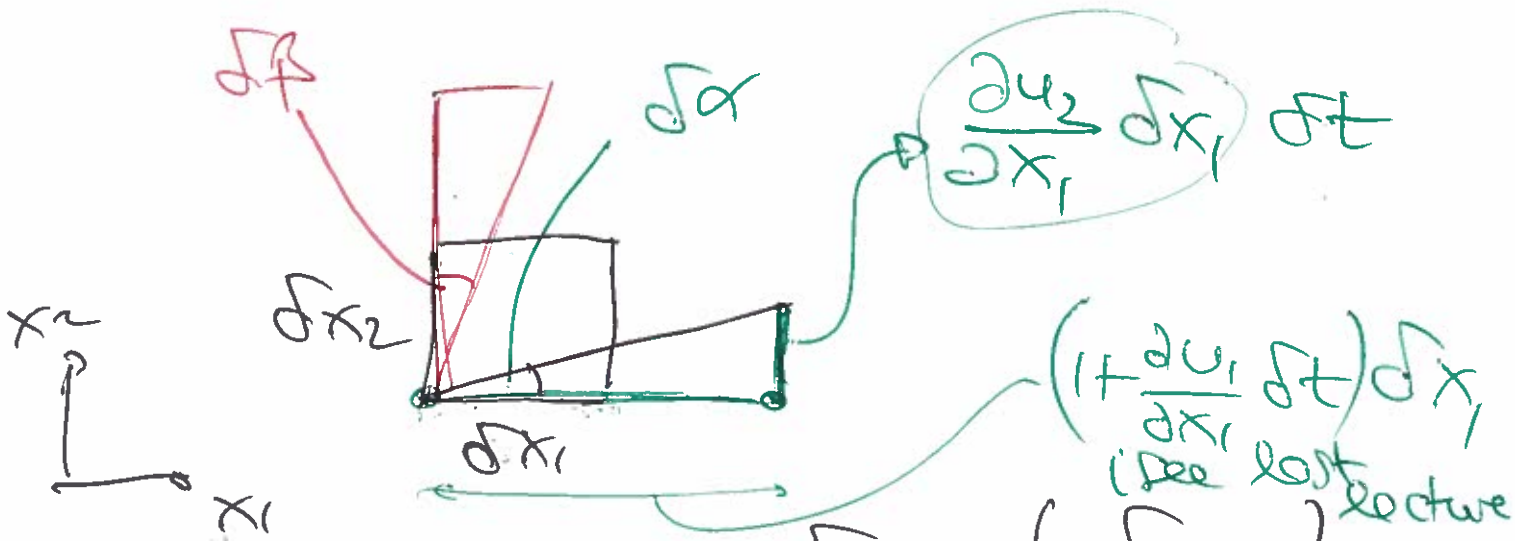
(ii) Shear rate of strain

~~Ques~~

# Illustration

(2D)

(2)



Compare lines  $dx_1$ , ( $dx_2$ ) after a short time interval  $dt$ . In sketch move end point on the left back to original posn.

$$\tan(dx) = \frac{\frac{du_2}{dx_1} dx_1 dt}{\left(1 + \frac{du_1}{dx_1} dt\right) dx_1}$$

Now  $dt \rightarrow 0$ ;  $dx \rightarrow 0$

$$\tan(dx) \rightarrow dx$$

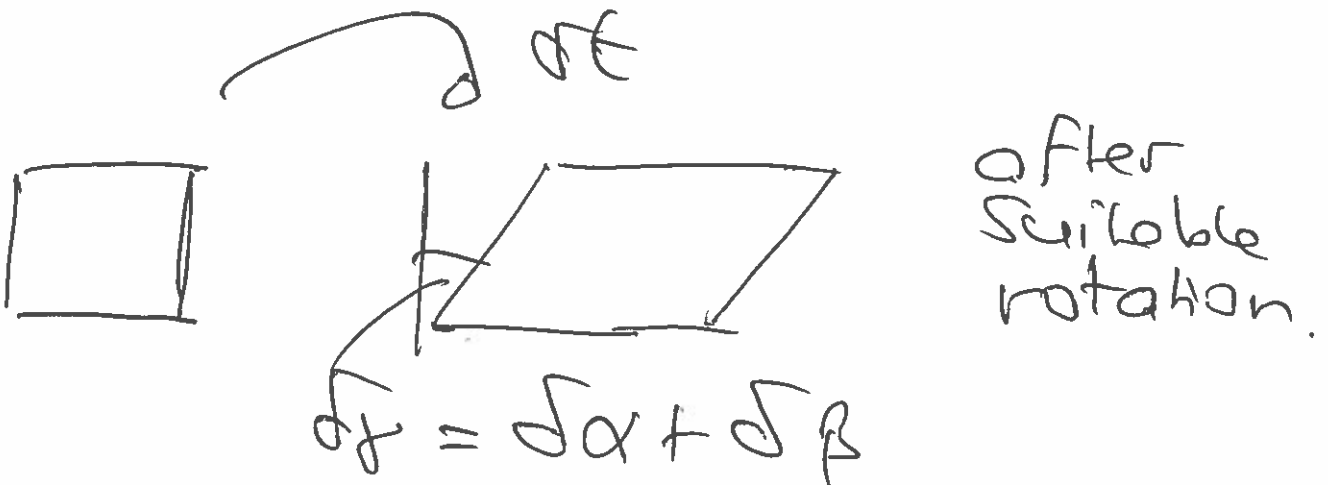
$$dx = \frac{du_2}{dx_1} dt$$

$$\frac{Dx}{Dt} = \frac{du_2}{dx_1}$$

Similarly:

$$\frac{D\beta}{Dt} = \frac{\partial u_1}{\partial x_2}$$

Now consider the "shear rate", i.e. the rate at which the angle between the two initially orthogonal lines changes:



$$\begin{aligned} \frac{D\gamma}{Dt} &= \frac{D\alpha}{Dt} + \frac{D\beta}{Dt} = \frac{\partial u_2}{\partial x_1} + \frac{\partial u_1}{\partial x_2} \\ &= 2\epsilon_{12} \end{aligned}$$

The off diagonal entries in  $\epsilon_{ij}$  represent half the shear rate in the  $x_i, x_j$ -plane.

Summary:

Motion of fluid in the vicinity of a point can be decomposed:

$$\underline{u}(x + \underline{dx}) = \underbrace{\underline{u}(x)}_{\text{translation}} + \underbrace{\underline{\Omega} \times \underline{dx}}_{\text{rotation}} + \underbrace{\underline{E} \underline{dx}}_{\text{deformation}}$$

fluid body

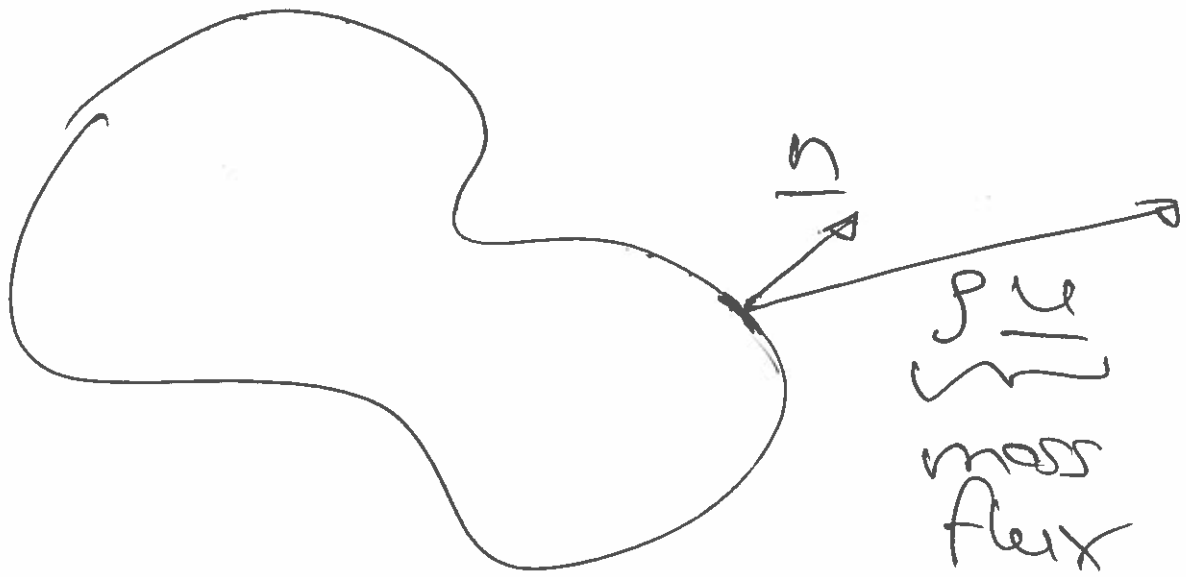
deformation:  
dilatation & shearing.

Equation of continuity

Physics: Mass flux into a spatially fixed (control) volume = rate of change of mass in that volume.

# Integral form:

5



$\rho = \text{density} \rightarrow \left( \frac{\text{kg}}{\text{m}^3} \right)$

$$\oint \rho \underline{u} \cdot \underline{n} dA = \frac{d}{dt} \int \rho dV$$

total mass flux over the boundary

mass inside volume

$$\frac{\text{kg}}{\text{m}^3} \frac{\text{m}}{\text{sec}} \text{m}^2 = \frac{1}{\text{sec}} \frac{\text{kg}}{\text{m}^3} \text{m}^3$$



$$\frac{d}{dt} \int \rho dV + \oint (\rho \underline{u}) \cdot \underline{n} dA = 0$$

divergence theorem

$$\int \frac{d\rho}{dt} dV + \int \nabla \cdot (\rho \underline{u}) dV = 0$$

$$\int \left[ \frac{d\rho}{dt} + \nabla \cdot (\rho \underline{u}) \right] dV = 0$$

For any fixed volume.

$\Rightarrow$  integrand must be zero!

$$\frac{d\rho}{dt} + \nabla \cdot (\rho \underline{u}) = 0$$

(differential form)

(continuity eqn.)

$$\frac{d\rho}{dt} + \frac{\partial}{\partial x_j} (\rho u_j) = 0$$

$$\underbrace{\frac{D\rho}{Dt} + u_j \frac{\partial \rho}{\partial x_j}} + \rho \frac{\partial u_j}{\partial x_j} = 0 \quad (2)$$

$$\left[ \frac{D}{Dt} = \frac{\partial}{\partial t} + u_j \frac{\partial}{\partial x_j} \right]$$

$$\underbrace{\frac{D\rho}{Dt}} + \rho \frac{\partial u_j}{\partial x_j} = 0$$

rate of  
change of  
density of  
fluid particle :

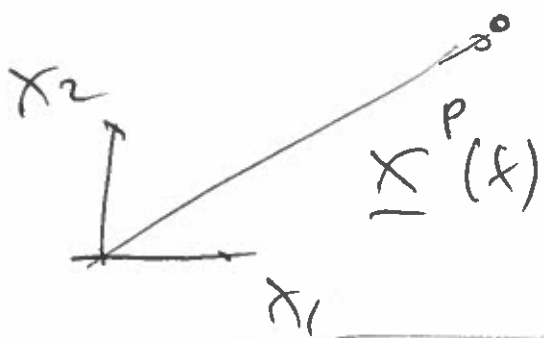
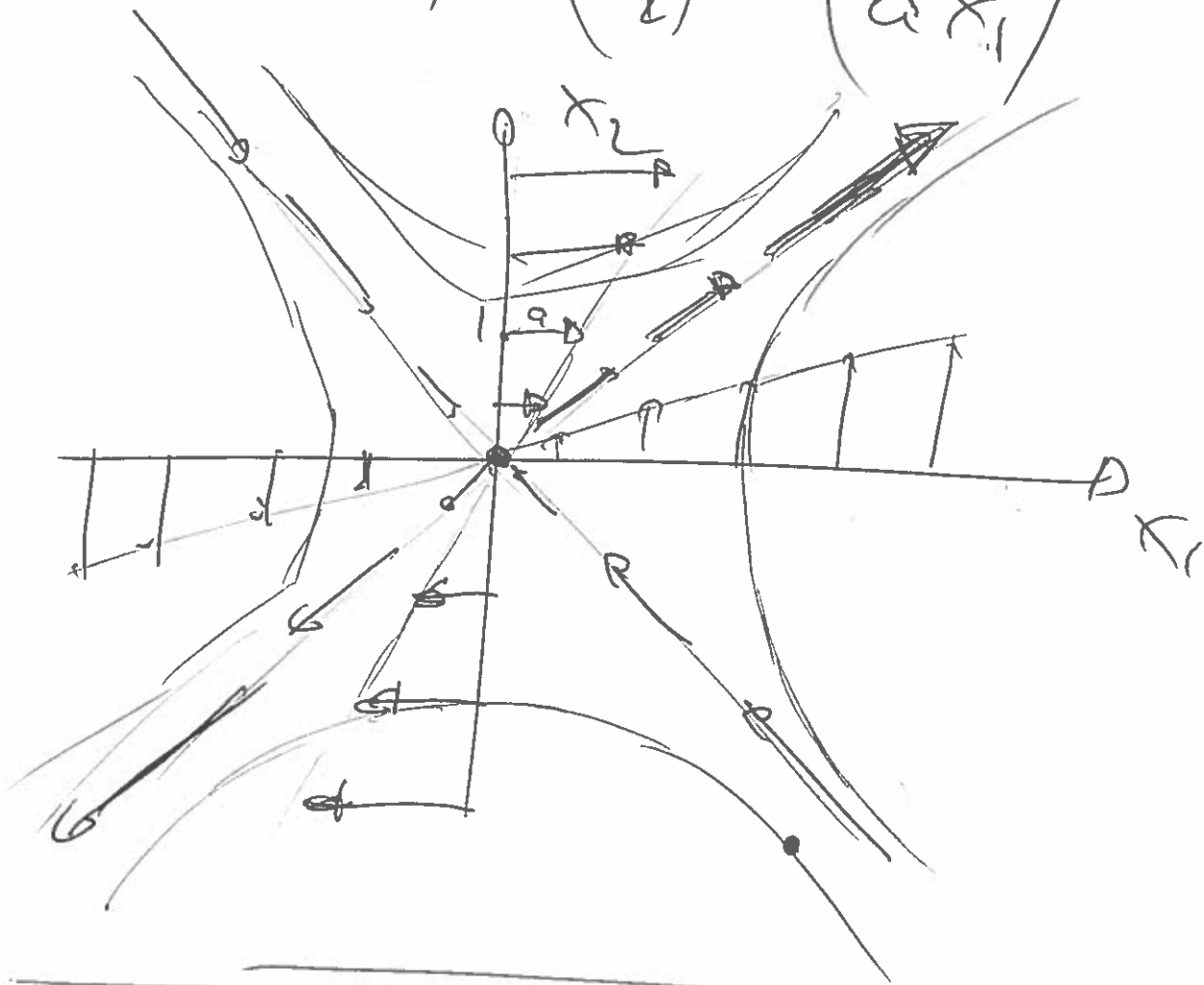
zero for  
incompressible  
fluids.

For such fluids the velocity  
field has to satisfy

$$\boxed{\frac{\partial u_j}{\partial x_j} = 0 \quad = \text{div. } \underline{u}}$$

This is a kinematic constraint!

$$u(x_1, x_2) = \begin{pmatrix} u_1 \\ u_2 \end{pmatrix} = \begin{pmatrix} ax_2 \\ ax_1 \end{pmatrix}$$



$$\frac{dx_i^p}{dt} = u_i(x_1^p, x_2^p)$$

$$\begin{aligned} \frac{dx_1^p}{dt} &= ax_2^p & x_1^p(t=0) &= X_1 \\ \frac{dx_2^p}{dt} &= ax_1^p & x_2^p(t=0) &= X_2 \end{aligned}$$



$$\frac{d^2 x_2}{dt^2} = a \frac{dx_1}{dt} = a^2 x_2$$

from 1<sup>st</sup> ODE

$$\frac{d^2 x_2}{dt^2} - a^2 x_2 = 0$$

$$x_2(t) = A e^{at} + B e^{-at}$$

IC:  $x_2(t=0) = X_2$

$$\left. \frac{dx_2}{dt} \right|_{t=0} = a x_1 \Big|_{t=0} = a X_1$$