

$$\begin{aligned}
 x &= L \\
 y &= h_0 \\
 u &= u \\
 v &= v = \left(\frac{h_0}{L}\right) u
 \end{aligned}$$

$$\begin{aligned}
 t &= \sqrt{15} \\
 p &= p
 \end{aligned}$$

$$h_0 \ll L \quad \left| \frac{\partial h}{\partial x} \right| = O\left(\frac{h_0}{L}\right) \ll 1$$

X-NSF:

$$\frac{\rho u h_0}{\mu} \frac{h_0}{L} \frac{\partial u}{\partial t} = - \frac{\rho}{\mu} \left(\frac{h_0}{L}\right) \frac{\partial^2 p}{\partial x^2} + \left[\frac{h_0}{L} \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 v}{\partial x^2} \right]$$

So if $Re\left(\frac{h_0}{L}\right) \ll 1$:

$$0 = - \frac{\rho}{\mu} \left(\frac{h_0}{L}\right) \frac{\partial^2 p}{\partial x^2} + \frac{\partial^2 v}{\partial x^2}$$

Aside:

$u(x)$



$$\frac{\partial u}{\partial x} = ?$$

$u = u(x)$
 $x = L$

$$\frac{\partial u}{\partial x} = \frac{\partial}{\partial x} \left(\frac{u}{L} \right)$$

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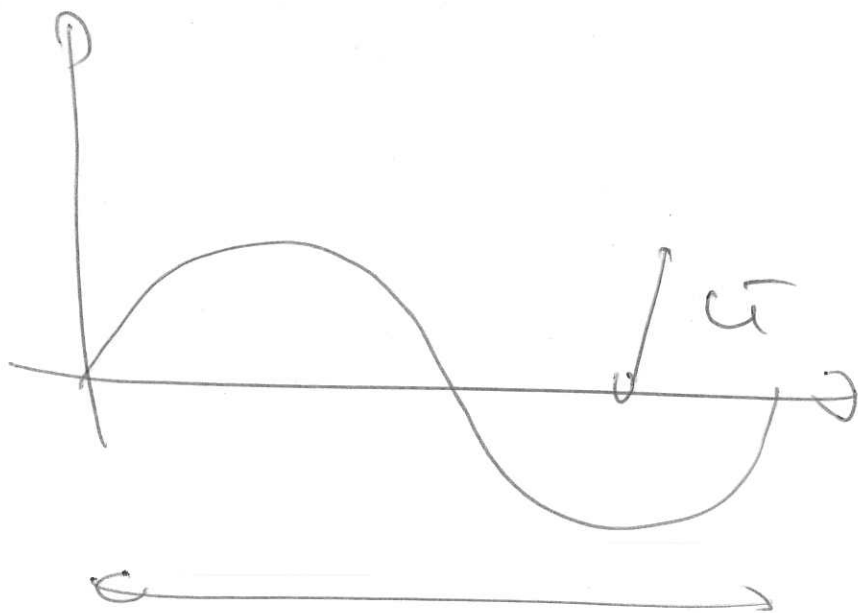
$$\frac{\partial u}{\partial x} = \frac{1}{L} \frac{\partial u}{\partial x} = 0$$



Specific example.

(3)

$$u(x) = U \sin\left(\frac{2\pi x}{L}\right)$$



$$\frac{du}{dx} = \frac{U}{L} 2\pi \cos\left(2\pi \frac{x}{L}\right)$$

$O(1)$

$$\frac{du}{dx} = O\left(\frac{U}{L}\right)$$

End
aside

This leaves a balance between the pressure gradient & viscous resistance. The terms balance if

$$\underbrace{\rho}_{\text{typical}} = \underbrace{\frac{\mu u}{h_0}}_{\text{shear stress}} \cdot \underbrace{\frac{1}{\left(\frac{h_0}{L}\right)}}_{\gg 1}$$

$$0 = -\frac{\partial \tilde{p}}{\partial x} + \frac{\partial^2 u}{\partial y^2}$$

Exercise:

y-mom. eqn.

$$0 = \frac{\partial^2 p}{\partial y^2}$$

= parallel flow eqns! (5)

Back to dim. form.

$$\left. \begin{aligned} 0 &= -\frac{dp}{dx} + \mu \frac{d^2 u}{dy^2} & (1) \\ \frac{dp}{dy} &= 0 & (2) \end{aligned} \right\}$$

BC: ~~u~~ $u(y=0) = 0$

$$u(y=h(x,H)) = U$$

Integrate (1) w.r.t. y :

$$u = \frac{1}{2\mu} \frac{dp}{dx} y^2 + Ay + B$$

const.

~~Apply~~ Apply BC.

$$u(x, y, t) = \frac{1}{2\mu} \frac{dp}{dx} (y^2 - hy) + \frac{U}{h}$$

press driven
flow



shear
flow



$h(x, t)$

⇒ Flow is parallel flow
in a channel with the
local width.

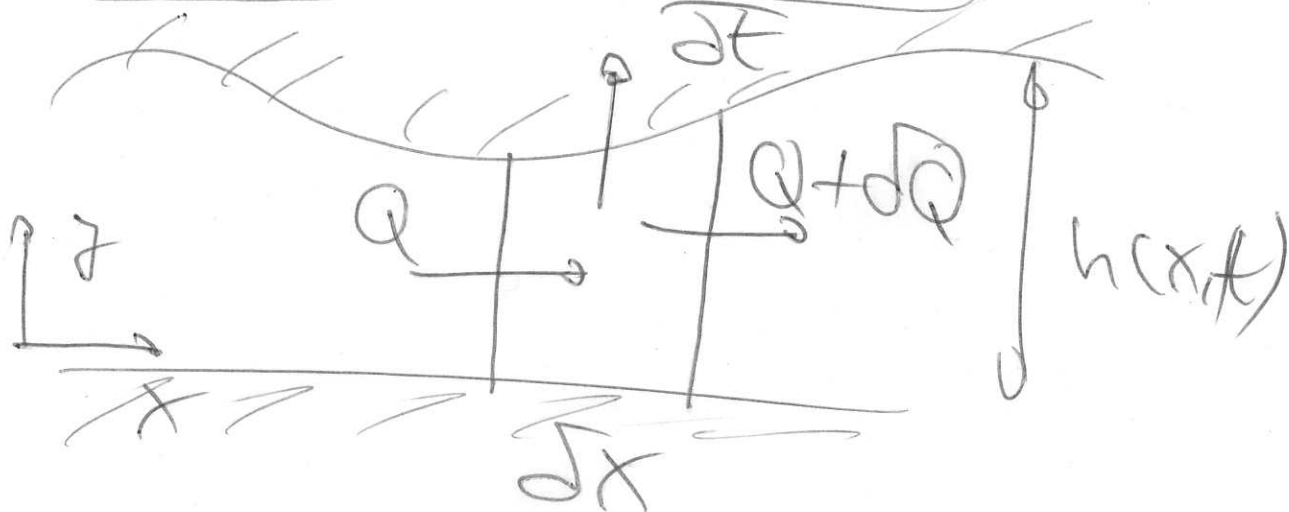
BUT: what is $\frac{dp}{dx}$?

Mass conservation has not
yet been enforced!

Consider volume flux through arbitrary cross section:

(2)

$$Q(x) = \int_0^{h(x)} u dy$$



Net outflow:

$$\Delta Q + \frac{dh}{dt} \Delta x = 0$$

as $\Delta x \rightarrow 0$,

$$\frac{dQ}{dx} = - \frac{dh}{dt}$$

$$Q(x) = \int_0^h u \, dy$$

\downarrow
 (A)

(8)

$$Q(x) = -\frac{1}{12\mu} \frac{\partial p}{\partial x} h^3 + \frac{1}{2} u h$$

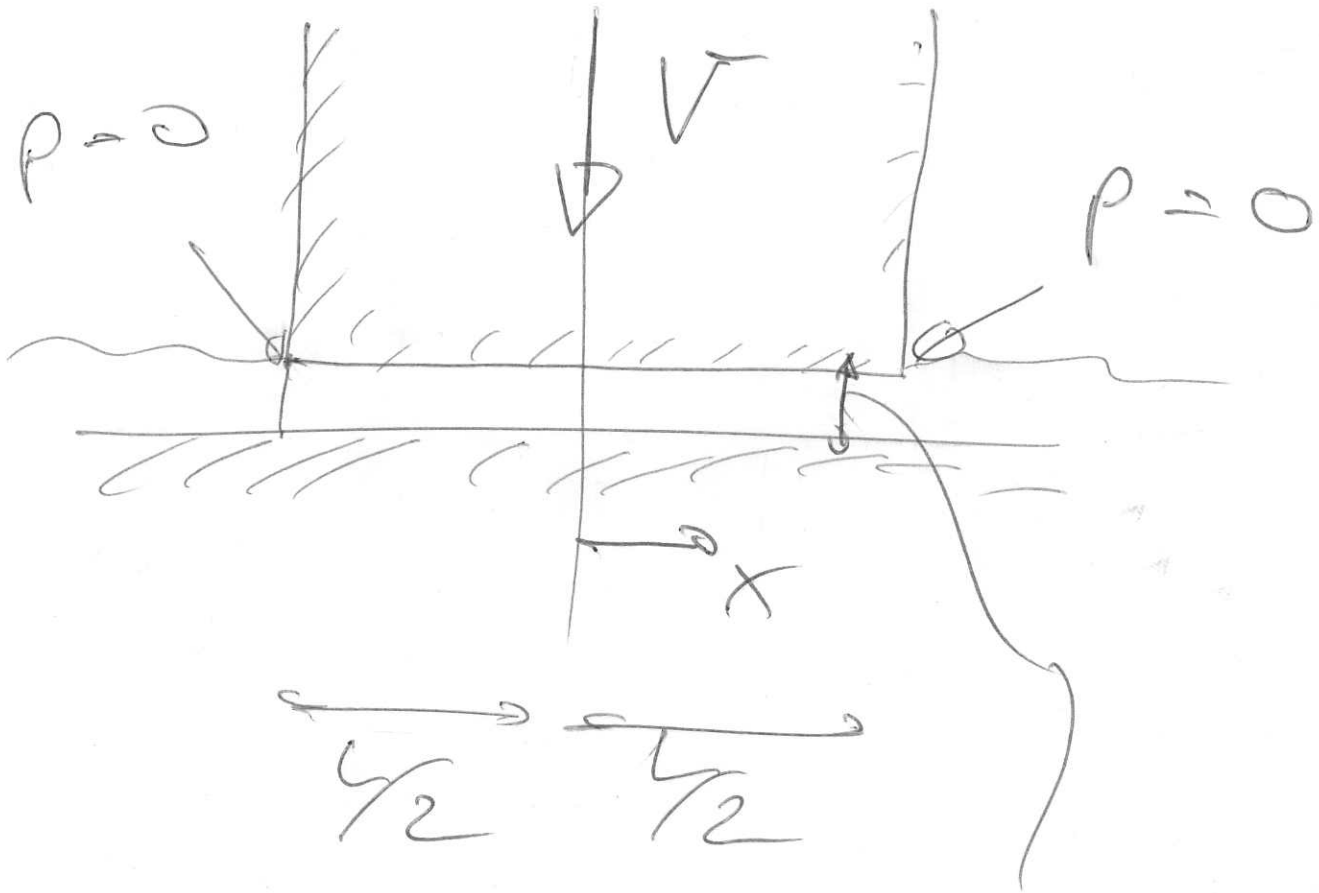
$$\frac{\partial Q}{\partial x} = \frac{\partial}{\partial x} \left(-\frac{1}{12\mu} \frac{\partial p}{\partial x} h^3 + \frac{1}{2} u h \right) = -\frac{dh}{dx}$$

$$\frac{\partial}{\partial x} \left(\frac{h^3}{\mu} \frac{\partial p}{\partial x} \right) = 12 \frac{dh}{dx} + 6 u \frac{\partial h}{\partial x}$$

Reynold's eqn. of
lubrication.

This is an eqn. for $p(x,t)$
veloc. follows from (A).

Example: Squeeze Film (9)



$h_0 \ll L$.

$$h(x,t) = h_0 - Vt$$

$$\frac{\partial h}{\partial x} = 0$$

$$\frac{\partial h}{\partial t} = -V$$

$$\frac{\partial}{\partial x} \left(\frac{h^3}{\mu} \frac{\partial p}{\partial x} \right) = 12 \frac{\partial h}{\partial t}$$

(10)

$$\frac{h^3}{\mu} \frac{dp}{dx} = -12\sqrt{x} + \tilde{A}(t)$$

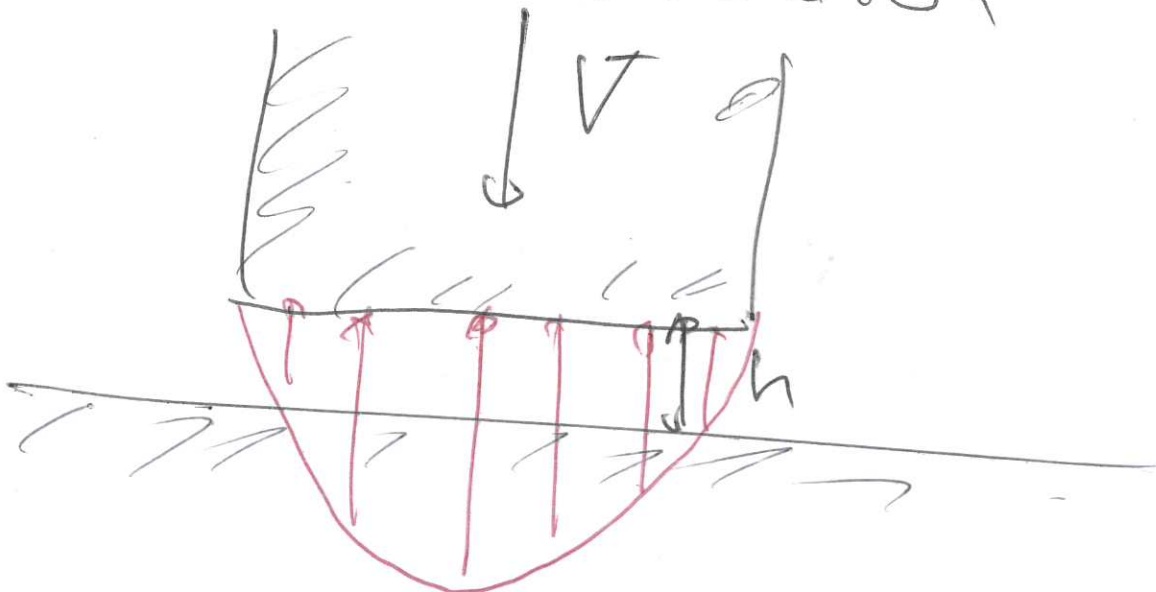
$$\frac{dp}{dx} = -\frac{12\sqrt{x}\mu}{h^3} + A(t)$$

$$p(x,t) = -\frac{12\sqrt{x}\mu}{h^3} \frac{x^2}{2} + A(t)x + B(t)$$

BC: $p(x = \pm \frac{L}{2}, t) = 0$

$$p(x,t) = -\frac{6\sqrt{x}\mu}{h^3} \left(x^2 - \left(\frac{L}{2} \right)^2 \right)$$

Note: Parabolic press distribution



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Note:

$p \rightarrow \infty$ as $h \rightarrow 0$.