

$$\underline{F} = F_x \underline{e}_x + F_z \underline{e}_z$$

$$F_x = g \sin \alpha \quad F_z = -g \cos \alpha$$

- Assume:
- parallel flow in  $x$ -dir
  - steady
  - indep. of  $z$

$$\cancel{\rho \frac{dv_x}{dt}} = -\frac{dp}{dx} + \underbrace{\rho g \sin \alpha}_{F_x} + \mu \left( \frac{d^2 v_x}{dy^2} + \cancel{\frac{d^2 v_x}{dz^2}} \right)$$

$$\boxed{0 = -\frac{dp}{dx} + \mu \frac{d^2 v_x}{dy^2} + \rho g \sin \alpha} \quad (1)$$

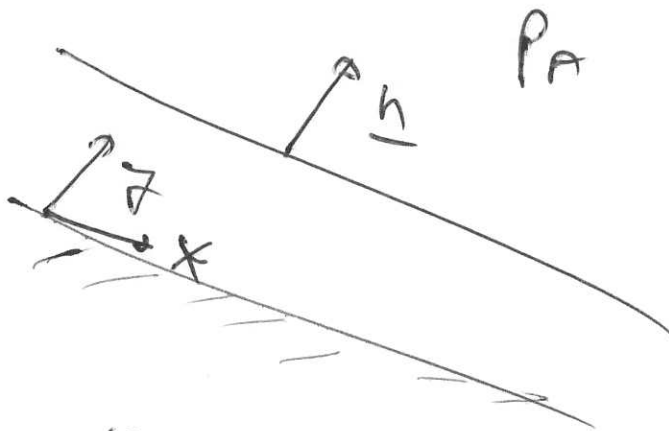
$z$ -comp:

$$\boxed{0 = -\frac{dp}{dz} - \rho g \cos \alpha} \quad (2)$$

BC:  $u(y=0) = 0$  (no slip)

At  $y=h$ : free surface; fluid meets (inviscid) air of a pressure  $p_A$ .

Surface of fluid is subject to an applied traction from the air



$$\underline{n} = n_x \underline{e}_x + n_z \underline{e}_z = \underline{e}_z$$

$$n_x = 0$$

$$n_z = 1$$

Traction on fluid

$$\underline{t} = -p_A \frac{\underline{n}}{|\underline{n}|} = t_x \underline{e}_x + t_z \underline{e}_z$$

$$t_x = 0$$

$$t_z = -p_A$$

In index notation:

$$n_1 = 0$$

$$n_2 = 1$$

$$t_1 = 0$$

$$t_2 = -p_A$$

Traction BC:

$$t_i = \tau_{ij} n_j \quad \text{at } z = x_2 = h$$

$$t_i = \left[ -p \delta_{ij} + \mu \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \right] n_j$$

$$t_i = -p n_i + \mu \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) n_j$$

for all 2 indices  $i = 1, 2$

$i = 2$ :

$$t_2 = -p n_2 + \mu \left( \frac{\partial u_2}{\partial x_1} + \frac{\partial u_1}{\partial x_2} \right) n_1$$

$$+ \mu \left( \frac{\partial u_2}{\partial x_2} + \frac{\partial u_2}{\partial x_2} \right) n_2$$

$u_2 = 0$  (parallel flow)

$$p = p_A \quad \text{at } x_2 = z = h$$

$i > 1$ :

$$t_1 = -\rho n_1 + \mu \left( \frac{\partial u_1}{\partial x_1} + \frac{\partial u_1}{\partial x_2} \right) n_1$$
$$+ \mu \left( \frac{\partial u_1}{\partial x_2} + \frac{\partial u_2}{\partial x_1} \right) n_2$$

$u_2 = 0$

$$0 = \mu \frac{\partial u_1}{\partial x_2} = \mu \frac{\partial u}{\partial y} \quad \text{at } y = h$$

Interpret (2) w.r.t  $y$ :

$$\frac{\partial p}{\partial y} = -\rho g \cos \alpha$$

$$p(x, y) = -\rho g \cos \alpha y + f(x)$$

Apply press. BC:

$$p(y=h) = p_A = -\rho g \cos \alpha h + f(x)$$

$$p(x, y) = p_A + \rho g \cos \alpha (h - y)$$

Note:

- press. increases through thickness of film (hydrostatics)

- press. does not depend on  $x$ :  
Flow not driven by press. but by gravity.

Now (1)

$$0 = -\cancel{\frac{dp}{dx}} + \rho g \sin \alpha + \mu \frac{d^2 u}{dy^2}$$

integrate twice w.r.t.  $y$ :

$$u = -\frac{1}{2} \frac{\rho g \sin \alpha}{\mu} y^2 + Ay + B$$

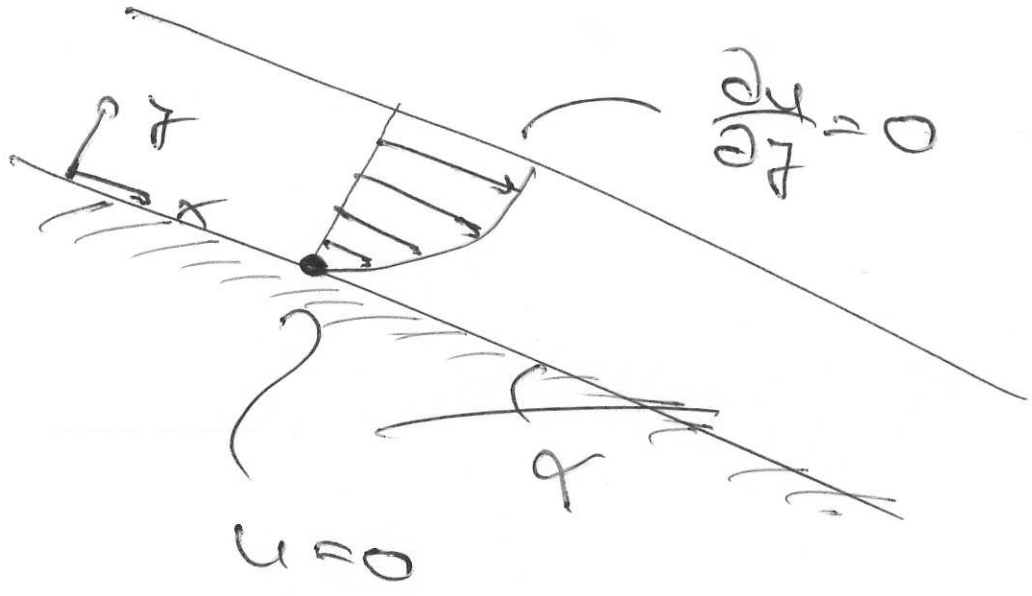
const.

Apply BC:

$$u(y=0) = 0$$

$$0 = \mu \frac{du}{dy} \Big|_{y=h}$$

$$u(x, y) = \frac{g \sin \alpha}{\nu} \left[ h y - \frac{1}{2} y^2 \right]$$



Example: The vibrating plate

fluid



$U \cos(\omega t)$

Assume:

- parallel flow
- flow driven by wall  $\Rightarrow$  no need for press. gradient.  $\frac{dp}{dx} = C = 0$
- no body force.

$$\rho \frac{\partial \psi}{\partial t} = -\cancel{\frac{\partial \psi}{\partial x}} + \cancel{\rho f_x} + \mu \left( \frac{\partial^2 \psi}{\partial y^2} + \cancel{\frac{\partial^2 \psi}{\partial z^2}} \right)$$

$$\boxed{\frac{\partial u}{\partial t} = \nu \frac{\partial^2 u}{\partial y^2}}$$