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Biodegradable composite scaffolds with an interconnected spherical network for bone tissue engineering

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Abstract

Tissue engineering scaffolds are highly engineered structures that accommodate cells, facilitate their expression, and resorb to facilitate regeneration of tissue. Anew technique for producing controlled pore shape and pore size interconnectivity offers promise for application as a tissue engineering scaffold. Salt particles were spheroidized in a flame and sintered to provide an interconnecting salt template. The salt template was filled with a carbonated fluorapatite powder and a polylactic polymer to produce a composite scaffold. It was found that a higher pore space is possible with the use of spherical and larger salt particle sizes. This technique can produce scaffolds with good interconnectivity and be suitable for producing pore size graded bodies. \odot 2004 Elsevier Ltd. All rights reserved.

Keywords: Scaffold architecture; Template; Pore connectivity; Pore shape; Salt leaching; Bone tissue scaffold

1. Introduction

Tissue engineering, the use of living cells together with either natural or synthetic [extra](#page-7-0)cellular components for implantable components and devices [1] is continually being developed to meet t[he](#page-7-0) increasing demand for tissue and organ substitutes. The disadvantage of autografts and allografts [2–4] and the shortage of donors has placed emphasis on synthetic means of reconstructing tissue and organs [5]. This process relies on the correct selection of bioresorbable materials in concert with a cell culture that together can produce a suitable biological tissue for implantation. Growth of a tissue or organ requires a cell culture seeded onto a support for cell growth and differentiation. This may be initiated outside the body, in a bioreactor or by the implantation of a porous scaffold inside the body. These cell-populated structures are not immediately functional and cannot immediately restore the vital functions of the implantable site in the body. Filling of the scaffold with a new tissue and the resorption speed of the scaffold must be balanced to provide the optimum tissue formation conditions.

The growth of tissue engineering has provided a platform for introducing a highly engineered pore network i[n e](#page-7-0)stablished biomaterials to form scaffolds. Certain characteristics were established early from the use of porous biomaterials [as](#page-7-0) a means of fixation. Pores needed to be greater than $100 \,\mu m$ for bone tissue ingrowth [6]. Studies on corals revealed that pore connectivity was necessary for deeper tissue growth within the porous body [7]. These channels allowed the supply of oxygen and nutrients to cells inside the scaffold and facilitated waste transfer out of the scaffold. The requirement of pore size and connectivity were thus quickly established for scaffolds.

Tissue growth will be implant site specific, dictated by the growth conditions, and also by the type of tissue being regenerated. The speed of tissue growth can be greatly influenced by biomaterial factors. Abiomaterial must resorb at a sufficiently high rate to accommodate the new tissue. Tissue growth will be implant site specific, dictated by the growth conditions, and also by the type of tissue being regenerated. The degradation products may further influence cell differentiation and health and thus a good knowledge of the degradation products is essential for selection of biomaterials in scaffold applications. Unlike other implants, where the degradation products may be removed by the surrounding fluid flow, the pore network within a scaffold cannot

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Fig. 1. Scaffold from a template made from angular salt particles.

offer as high a fluid exchange and thus cells are expected to be more sensitive to the degradation products of biodegra[dab](#page-7-0)le scaffold materials. Calcium phosphates dissolve to produce phosphate and calcium, both of which are widely distributed in the body, needed for cellular function, and are thus suitable for use in scaffolds [8]. The brittle nature of calcium phosphates can be overcome by incorporating the calcium phosphates with polymeric materials, analogous to the composite nature of bone.

The physical characteristics of a [sca](#page-7-0)ffold can be described by an average pore size, the pore size distribution, pore volume, pore interconnectivity, pore shape, po[re th](#page-7-0)roat size and pore roughness. Aminimum pore size is required for tissue growth [9], interconnectivity for access to nutrients and transport of waster products, pore shape and roughness for better cell spreading [10] and pore throat size for passage of tissue throughout the scaffold. The physical aspects of scaffolds are typically dictated by the choice of manufa[ctur](#page-7-0)ing process. Placement of different chemical compounds or growth factors within the scaffold walls or adsorbed to the pore walls can further enrich the scaffold to prom[ote](#page-7-0) cellular behaviour or t[issue](#page-7-0) growth [11].

The range of scaffold manufacturing techniques is the most diverse for polymers covering the use of porogens, chemical segregation [12] and rapid prototyping [13]. Porogens represent a common approach for introducing porosity with freeze drying, salt leaching or dissolution of salt templates. Isolated ice particles are joined as sublimation provides pore interconnectivity. Salt leaching is limited to polymers, due to the low interconnectivity of particles randomly assembled in a biopolymer dissolved with a solvent. Pores are dictated by the salt particles and are typically angular. Chemical segregation offers the ability to control the pore morphology as one phase is removed with a solvent. Rapid prototyping, including processes such as fused deposition modelling, selective laser sintering, stereolithography and threedimensional printing, are able to control the pore size and interconnectivity very effectively, but cannot control other aspects such as pore shape and roughness. All the above-mentioned techniques are capable of producing scaffolds and are very often used in conjunction with another technique to enhance the pore characteristics.

Salt leaching is a very simple ap[proa](#page-7-0)ch but is limited in the control of pore shape and connectivity. Initial work revealed limited pore interconnectivity produced with loosely packed salt particles [14]. The low probability of pore intercon[necti](#page-7-0)vity limited the [scaffold](#page-7-0) size to a thickness of 3 mm. This limitation was overcome by producing interparticle connections that has been possible by placement of the salt particle arrangement in a humid atmosphere [15] or by sintering [16,17]. The resulting polymeric scaffold that can be formed from the connected salt template is illustrated in Fig. 1.An enlarged view illustrates connecting channels at the base of a pore, with adjacent pores. The purpose of this work is to investigate the use of spherical salt particles to produce templates with an improved pore shape, good pore interconnectivity, reproducible pore throat size that can be used for producing a load bearing composite scaffold for cell seeding in bone tissue engineering applications.

2. Materials and methods

2.1. Apatite synthesis

Carbonated fluorapatite with the composition of $Ca_{9.223}Na_{0.518}(PO_4)_{5.223}(CO_3)_{0.777}F_{1.741}$ was synthesized by adding di-ammonium hydrogen phosphate with sodium bicarbonate and sodium fluoride at a rate of 10 ml/min into a calcium nitrate solution at 37° C. The pH in the calcium solution was adjusted to 9.4 with a pH

stat (Titrino 736, Metrohm, Switzerland) after which addition of the phosphate solution commenced. During the reaction, the pH was continuously adjusted to 9.4 to ensure constant pH conditions during the synthesis. The obtained powder was filtered, washed, dispersed in ethanol and dried for $12h$ at 104° C. The powders were then calcined using a heating rate of 10° C/min until 500° C and then maintained at temperature for 2 h. The characteristics of this powder are available elsewhere. X-ray diffraction (XRD) patterns were collected from $10-2\theta$ to $90-2\theta$ using a Rigaku Geigerflex diffractometer with Bragg–Bentano geometry in a step mode with a step size of 0.02° and 10 s per step using Copper $K\alpha$ radiation at 40 kV and 22.5 mA passing through a 0.5° divergence slit and 0.3° receiver slit.

Crystal size and lattice strain were calculated for (0 0 1) direction, using the Scherrer equation [16]. The formulae used for the calculations are:

Crystallite size
$$
C_s
$$

\n
$$
\equiv \frac{K \times \lambda}{W_{\text{size}} \times \cos \theta} \text{with } W_{\text{size}} = W_b - W_s,
$$

Lattice strain L_s

$$
\equiv \frac{W_{\text{strain}}}{4 \tan \theta} \text{with } W_{\text{strain}} = (W_b^2 - W_s^2)^{1/2},
$$

where K is the form factor assumed to be 0.9, λ wavelength, W_{size} is the broadening caused by small crystals, W_b is the broadened profile width, W_s is the standard profile width and W_{strain} is the broadening caused by lattice distortion.

2.2. Salt particle preparation

Sodium chloride rock salt with a mean size of 2 mm was ball milled for 1 min at 300 rpm in an alumina vessel and then sieved with a vibratory stack of sieves for 60 min to obtain powder within particle size ranges of $<$ 100, 100–150, 150–300, 300–500 and $>$ 500 µm. Salt was then dried in an oven at 120° C to remove any adsorbed moisture and facilitate particle packing when placed in a measuring cylinder to measure the packing volume. The salt weight and occupied volume were then used to determine the packing efficiency.

Salt was spheroidized by external injection into a Metco 5P (Sulzer Metco, Wohlen, Switzerland) flame spray torch at a rate of $1 g/min$ to optimize the heat transfer to the salt particles. Previous work has indicated that particles smaller than 150 mm are spheroidized effectively when the torch is used in the conventional manner [17]. Spheroidization of larger particles was investigated by increasing the dwell time and decreasing the particle velocity within the flame.

2.3. Template manufacture

Ten grams of sieved salt particles of different size ranges were placed in a 20 mm diameter alumina crucible for sintering. Sodium chloride spherical particles were sintered in a muffle furnace for 2 h. These salt templates were examined by scanning electron microscopy in a Hitachi S570 (Tokyo, Japan).

The packing density was assessed for particles and the sintered template. The packing density for particles was assessed by pouring particles into a measuring cylinder to fill a volume of 20 ml^3 and then weighing the powder needed to fill this volume. The salt assembly was placed on a vibratory base for 1 min to maximize particle packing. Template volume was determined by weighing the cylindrical pellet and then determining the dimensions of the pellet for a calculation of the density.

To assess the continuity of the salt network, epoxy resin was mounted into the porous salt block using vacuum impregnation. The epoxy was ground, and the salt dissolved in water to reveal the pore network in a scanning electron microscope.

2.4. Scaffold production

Asuspension of 17 g of apatite in 25 ml of pure ethanol was prepared with mechanical and ultrasonic agitation. Sodium chloride templates were soaked twice for 5 min in the apatite suspension while resident in an ultrasonic bath. The sodium chloride template with the apatite slurry was dried in an oven at 100° C for 3 h.

Poly(L -lactic acid), a weight of 0.2 g, was dissolved in 6 ml of $CH₃Cl$ and introduced into the apatite filled salt template by pouring over the template. The solvent was allowed to evaporate at room temperature for 24 h and then in vacuum at -100 kPa for an additional 24 h.

The 18 mm high template filled with apatite and polylactic acid was soaked in deionized water for 30 min to remove the interconnected salt template. After drying, the scaffold was fractured and examined in the scanning electron microscope.

3. Results

The yield from the milling and sieving operation provided 30% of the particles b[etwe](#page-7-0)en 150 and 300 μ m and another 30% larger than $300 \,\mu m$, Fig. 2. Previous investigations have indicated that particles smaller than $150 \mu m$ can be spheroidized effectively when the torch is used in the conventional manner [17]. Spheroidization of larger particles required the optimization of the spray conditions by increasing the dwell time and decreasing the particle velocity within the flame.

The flowability of salt particles changed with particle size exhibiting a decrease with smaller particle size. The

Fig. 2. Salt particle size distribution after communition.

Fig. 3. Particle packing of angular, spheroidized and sintered particles with a different size range.

poor flowability of smaller particles was accentuated with time as moisture was readily adsorbed onto the particle surface. Salt particles were initially dried in an oven to minimize the adsorbed moisture.

Particles less than $80 \mu m$ produced a packing density of 35%, Fig. 3. This increased significantly to 43% with the next particle size range $(80-106 \,\mu m)$. Larger particle size ranges only provided a small improvement in the packing, reaching a value of 48% for $300-500 \,\mu m$ particles.

Spherical particles produced by thermal spraying provided an increase in the packing density. A5% increase was noted for salt particles in the $106-150 \,\mu m$ range. The improvement in the packing density increased with particle size and reached a value of 59% for the 300– $500 \,\mu m$ particle size range. Sintering of the particle compact led to another increase in packing density, reaching a value of 62% for the $106-150 \,\mu m$ salt particles.

Salt particles sintered for 2 h produced a salt compact that could be handled with ease without causing fragmentation. The template could be removed from the alumina crucibles in a cylindrical form. A fracture surface was formed from the [sintered](#page-4-0) salt template to investigate the connectivity, and it was found that particles established a sound bond with surrounding particles placed in relative contact from the powder filling of the alumina crucibles, Fig. 4. The surface view of the $150-300 \,\mu m$ salt particles revealed underlying interconnected particles and a fracture surface which [displaye](#page-4-0)d good interconnectivity. Similarly, larger particles also exhibited good interconnectivity and the fracture revealed failure in the throat areas more commonly than through the core of the particle, Fig. 4b. Throat areas in the template made from salt particles larger than $500 \mu m$ were still observed, despite the more irregular packing provided by rounded parti[cles th](#page-4-0)at exhibited rough areas from the unmolten areas of particles.

The throat size/neck size produced between the separate salt particles exhibited an increase with particle size, Fig. 5. The neck size increased from $60 \pm 5 \,\text{\mu m}$ for $106-150 \,\mu m$ particles to $90\pm8 \,\mu m$ for $300-500 \,\mu m$ particles. This corresponds to a ratio of particle size to neck size of 3.8, 5 and 5.1 for the increasing particle size ranges. A large difference is apparent between the smaller particle sizes, but the small change with particles greater than $500 \mu m$ could be attributed to the rounded but non-spherical shape of the salt particles that did not facilitate good particle contact. The particle contact for well-packed particles clearly provides areas of a negative and positive curvature that act as sites for vaporized material deposition and removal.

The carbonated fluorapatite, consists of small crystallites with a crystal size of 326 A and a 64% crystal strain in the (001) direction resembling francolite. The small crystallites could readily fill the large pore spaces within the sintered salt template. Dispersion of the apatite in chloroform did not lead to any noticeable dissolution. This provided good transfer of the apatite particles into the pore space of the salt template. Drying of the filled salt template in an oven for 1 day ensured good solvent removal.

Chloroform as a solvent was chosen on the basis of readily dissolving the polylactic acid, not dissolving the apatite crystallites and the salt template. Separately drying the apatite filled scaffold followed by drying of the polylactic acid decreased the amount of solvent that could remain in the scaffold.

Pouring the dissolved polylactic acid over the apatite filled salt template filled the pore space and the area surrounding the scaffold. The o[uter lay](#page-5-0)er of the template was covered with a layer of apatite crystallites, and this remained on the surface of the scaffold, bound with the polylactic acid. This is observed as the fine-grained area on the right side of Fig. 6a. The polylactic acid that has penetrated into the pore space of

Fig. 4. Salt template consisting of (a) spherical 150–300 μ m particles, (b) spherical 300–500 μ m particles and (c) rounded $>$ 500 μ m particles.

Fig. 5. Neck size of sintered salt particles of different particle sizes.

the salt template filled the pore space to produce a scaffold structure. Higher magnification of the pore walls revealed that fine pores remained within the walls, and the polylactic acid exhibited a tendency to fill the space between the agglomerated apatite deposit and the salt template. This produced a structure of loosely agglo[merated apatite](#page-5-0) crystals within the pore walls, which was sealed with a layer of polylactic acid. The same distribution of the polylactic acid and apatite was observed with the template that contained a larger pore space, Figs. 6b and c.

4. Discussion

The pore space characteristics offered by the salt template are unique and different from other scaffold manufacturing processes. Sintering salt particles has produced an interconnected spherical pore network in the scaffold with the ability to control the throat size and pore wall characteristics.

The throat size is a function of the sintering conditions, a longer sintering time producing a larger throat size, and thus providing a template with larger interconnecting regions. This can produce a scaffold with less fluid flow resistance, that can be an advantage when filling the template during the scaffold manufacture

Fig. 6. PLLA reinforced apatite scaffolds manufactured from scaffolds using (a) 150–300 µm salt particles, (b) 300–500 µm salt particles and (c) $>500 \,\mu m$ salt particles. An enlarged view of (a) is shown in (d).

but also for easier stem cell placement and improved fluid transport throughout the scaffold when implanted in the body.

The time for establishing the sintered necks was significantly lower than that required for sintering angular particles. This is attributed to the stress condition within the spherical salt particles compared to the angular particles. Small salt particles are completely molten, whereas larger salt particles are only molten in the outside shell. Solidification will commence from the outside for the smaller particles, but from the core of partially molten larger particles. The shell on smaller molten droplets solidifies first and creates a rigid surface for further solidification. The contraction from the liquid to solid leads to the presence of voids within the spheres, but also places the shell in a compressive residual stress condition. Larger particles will have the shell in a tensile residual stress condition as the molten shell solidifies. These residual stress conditions provide stored energy that hastens the sintering process compared to angular particles. The observation of a larger throat size in the larger particles could be attributed to a higher stress condition in the solidified [salt](#page-7-0) particles.

Salt particles experience very little densification attributed to the evaporation–condens[ation](#page-7-0) process as the governing sintering mechanism within halides [18]. The amount of densification decreases 10-fold from 20% for 38 μ m particles to 1% for 100 μ m particles under the same sintering conditions [19]. The 20% improvement in the packing density could thus be explained by the other sintering mechanisms playing a more important role in the sintering of thermally sprayed particles. This is thought to arise from the higher ionic mobility within the salt structure attributed to the high defect concentration that is characteristic for rapidly solidified materials. The use of longer sintering times is expected to be a good means of increasing the salt packing density to values higher than 62%. The longer sintering time would be expected to produce wider throat sizes and higher packing densities. This is an advantage in those situations where mechanical loads

do not need to be supported, allowing the use of a higher pore conte[nt sc](#page-7-0)affold.

Aunique surface feature that occurs as a result of the evaporation–condensation sintering mechanism is the appearance of ledges surrounding the point of low curvature [16]. Given that the surface profile is reproduced in the scaffold, these fine ledges ca[n be](#page-7-0) used to an advantage for tissue guidance and provide a surface for good cell attachment. It has previously been shown that fine grooves can be useful for controlling the direction of cellular migration over a surface [20] and can be used for faster filling of the interior scaffold surface. Since a surface with roughness is important for cell expression, the combination of a roughness and directional ridges can be important aspects for controlling the speed of cell guidance and resulting tissue growth with the scaffold. The spherical pore shape will act as the ideal surface for the ridges by providing a surface for [ease](#page-7-0) of cell spreading, unlike an angular pore that will suspend cell movement within the scaffold.

This technique has shown that salt leaching is no longer limited by a 3 mm thick scaffold as previously set by Mikos [14]. Interconnected pore networks can be manufactured to any desired scaffold size sintering an assembly of salt spheres. Sintered angular particles produce a low packing density, a broad range in pore throat size and thus an inhomogeneous distribution of similar pore throat sizes within the scaffold. This is a result from the wide range of particle assembly configurations, Fig. 7. The largest throat size can be produced when the face of one angular particle resides adjacent to another particle, however the chances of this configuration are very low in comparison to a particle corner abutting onto the corner, side or face of another particle. The use of angular particles is not a sound means of producing a uniform throat size throughout the scaffold. This can only be established with the use of spherical salt particles that will also exhibit a better packing efficiency.

Other scaffold manufacturing approaches may be used in parallel with the described technique. The use of

two approaches in conjunction ha[s bee](#page-7-0)n used previously to increase the amount of open porosity within a scaffold, or to lead to a stiffer scaffold. Previous studies have shown than sections up to $300 \mu m$ may be stiffened using the gas foaming technique [21]. This is an ideal technique for increasing the stiffness of such scaffolds to [be s](#page-7-0)uitable for load bearing sites within the body. The pore walls can also be modified using a spinodal decomposition technique to introduce small pores between the larger pore spaces in the final scaffold [22]. These techniques when used in conjunction can tailor the pore architecture and material properties for enhanced performance. Other polymeric materials that are readily dissolved in a solvent such as chloroform can be used in this technique.

An attractive feature of this process is the ability to shape the salt template to the required geometry for implantation in the body. The sintered form can be easily ground to the desired shape. The internal pore architecture can be well controlled to produce a spherical pore shape, a desired pore size, pore throat size, and pore roughness. A graded pore structure and the inclusion of larger channels can be easily manufactured by assembly salt particles of different sizes. This innovative process provides control over a range of features that is not commonly available within scaffolds and offers great potential for bone tissue engineering where the scaffold strength and stiffness and strength can be further tailored with a composite and pore wall pore structure control.

5. Conclusion

Production of a salt template from spherical salt particles is a novel technique that offers pore interconnectivity, pore shape control, throat size design for scaffolds to be used in bone tissue engineering applications. It was found that spherical particles provide a higher pore volume scaffold than angular particles and can offer a more homogeneous pore size distribution throughout the scaffold.

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Fig. 7. Influence of particle shape on the neck characteristics.

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